(1) Publication number:

**0 350 970** A1

Q

### **EUROPEAN PATENT APPLICATION**

- (1) Application number: 89115775.2
- 2 Date of filing: 24.02.84

(a) Int. Cl.4: C12P 13/14 , C12N 1/20 , //(C12N1/20,C12R1:13,1:15)

- Priority: 25.02.83 JP 30480/83 22.09.83 JP 174319/83
- Date of publication of application: 17.01.90 Bulletin 90/03
- Publication number of the earlier application in accordance with Art.76 EPC: 0 117 740
- Designated Contracting States:
  DE FR GB

- Applicant: KYOWA HAKKO KOGYO CO., LTD. 6-1, Ohte-Machi 1-chome Chiyoda-ku Tokyo-to(JP)
- ② Inventor: Hattori, Kiyoji c/o Patent Department Kyowa Hakko Kogyo Co. Ltd 6-1 Ohtemachi Itchome Chiyoda-ku Tokyo(JP)

Inventor: Kotani, Yukinobu c/o Patent

Department

Kyowa Hakko Kogyo Co. Ltd 6-1 Ohtemachi

Itchome<sup>-</sup>

Chiyoda-ku Tokyo(JP)

inventor: Kino, Kuniki c/o Patent Department Kyowa Hakko Kogyo Co. Ltd 6-1 Ohtemachi

Itchome

Chlyoda-ku Tokyo(JP)

Representative: Lambert, Hugh Richmond et al D. YOUNG & CO. 10 Staple Inn London, WC1V 7RD(GB)

- Process for producing L-glutamic acid by fermentation and mutant microorganisms for use therein.
- A fermentation process is disclosed for producing L-glutamic acid in high yield using microorganisms belonging to the genus Corynebacterium or Brevibacterium having the ability to produce L-glutamic acid and which have or have been endowed with a resistance to one or more antibiotics of the type which inhibit energy metabolism and selected from oligomycin, antimycin A, rutamycin, and valinomycin.

EP 0 350 970 A1

# PROCESS FOR PRODUCING L-GLUTAMIC ACID BY FERMENTATION AND MUTANT MICROORGANISMS FOR USE THEREIN

The present invention relates to a process for producing L-glutamic acid by fermentation and microorganisms for use therein.

L-glutamic acid is an important amino acid which is commercially useful as a food additive.

Processes for producing L-glutamic acid by fermentation are known using strains of various microorganisms of the genera Corynebacterium and Brevibacterium in particular strains having a nutritional requirement for various compounds, or a sensitivity or resistance to various chemicals. The yields of these known processes are comparatively low and a need exists for processes for producing L-glutamic acid in higher yields at low cost.

As a result of various studies for obtaining strains having an increased L-glutamic acid productivity, it has been found that L-glutamic acid-producing microorganism strains of the genus Corynebacterium or Brevibacterium and endowed with a resistance to an antibiotic inhibiting energy metabolism have a remarkably improved ability to produce L-glutamic acid.

Accordingly, the present invention provides a process for the production of L-glutamic acid which comprises culturing a mutant having an ability to produce L-glutamic acid in a nutrient medium until L-glutamic acid is accumulated in the resulting culture liquor, and recovering L-glutamic acid therefrom wherein there is used a mutant belonging to the genus Corynebacterium or Brevibacterium and having a resistance to one or more antibiotics of the type which inhibit energy metabolism.

As used herein the term "antibiotics which inhibit energy metabolism" means that the antibiotics have influences on the electron transport of respiratory chain or oxidative phosphorylation. Examples of such antibiotics include inhibitors of the electron transport system such as antimycin A, uncoupling agents which allow electron transport to continue but prevent the phosphorylation of ADP to ATP, such as gramicidin S, valinomycin, etc., and inhibitors of oxidative phosphorylation which prevent the ATP-forming mechanism from utilizing the high-energy intermediate or state generated by electron transport, e.g. antibiotics such as oligomycin, rutamycin, etc.

In a second aspect the invention also extends to biologically pure cultures of the microorganisms per se.

25

30

Suitable mutants for use in this invention may be obtained by using a mutant inherently having an ability to produce L-glutamic acid or an improved mutant thereof as a parent strain and imparting thereto the specified resistance.

Alternatively, a suitable mutant may be prepared by a reverse process, i.e. by imparting the abovementioned ability to produce L-glutamic acid to a mutant already possessing a specified resistance.

The mutant microorganisms useful in carrying out the present invention can be obtained by conventional mutation techniques using for example mutagens such as ultraviolet ray irradiation, x-ray irradiation, radioactive ray irradiation and a treatment with chemical mutagens. Treatment with N-nitro-N'-methyl-N-nitrosoguanidine (hereinafter referred to as NTG) is the preferred technique.

In addition, the mutants used in this invention may well have or be endowed with other specific properties such as specific nutritional requirements, drug resistance, drug sensitivity and drug dependence, in addition to the resistance already specified.

Preferably, the mutants used in carrying out this invention may, in addition to a resistance to energy metabolism inhibitors, also have a resistance to  $\alpha$ -naphthoquinoline and/or a resistance to one or more compounds being compounds which are precursors in the biosynthesis of ubiquinone.

As used herein the term "precursors for ubiquinone biosynthesis" means that the precursors are biosynthetic intermediates of ubiquinone which plays an important role in the electron transport of respiratory chain for acquiring the energy. Exemplary of such precursors are o-hydroxycinnamate (o-coumarate) and its fluoride, m-hydroxycinnamate (m-coumarate) and its fluoride, phenyl pyruvate, p-hydroxyphenyl pyruvate and its fluoride, phenyl acetate, p-hydroxyphenyl lactate and its fluoride, cinnamate, benzoate, p-hydroxybenzoate and its fluoride, and p-hydroxybenzaldehyde and its fluoride.

Strains mutated as above mentioned are screened by culturing in a nutrient medium and a strain having the ability to produce L-glutamic acid in greater yields than its parent strain is selected and used in this invention. A specific example of the procedure for obtaining a suitable strain is given in the following description.

#### Procedure

Corynebacterium glutamicum ATCC-13032 or Brevibacterium lactofermentum ATCC-13869 is suspended in a M/20 phosphate buffer solution (pH 7.0). To the suspension is added 200 μg/ml NTG and the mixture is maintained at 30 °C for 30 minutes. The treated mutants are collected and washed with the same buffer solution. Then, the mutants are spread on a medium (pH 6.8) comprising 3% glucose, 0.2% urea, 10 ppm each of Fe, Mn and Cu ions, 1 mg/l thiamine hydrochloride, 50 μg/l biothin and 2% agar, and further containing 100 μg/ml oligomycin. Culturing is carried out at 30 °C for 2 to 20 days. Among these mutants, those having a remarkably improved ability of producing L-glutamic acid are separated. Typical examples of the oligomycin-resistant strains are Corynebacterium glutamicum COM-53 (hereinafter referred to as COM-53) (FERM BP-428) and Brevibacterium lactofermentum BOM-419 (hereinafter referred to as BOM-419) (FERM BP-429).

The strains COM-53 and BOM-419 were deposited on February 19, 1983 outside the Budapest Treaty with the Fermentation Research Institute, the Agency of Industrial Science and Technology, Japan, as FERP P numbers shown below. The deposits were converted into the deposits under the Budapest Treaty, and the corresponding international deposit numbers are shown below.

Strain	FERM P No.	FERM BP No.
COM-53	6921	428
BOM-419	6922	429

25

20

Either a synthetic or natural medium may be used as the medium for the present invention, so long as it properly contains a carbon source, nitrogen source, inorganic materials and other necessary nutrients which are assimilable by the strain utilized.

As the carbon source, various carbohydrates such as glucose, fructose, maltose, monnose, glycerol, sucrose, starch, starch hydrolyzate and molasses, sugar alcohols, such as glycerol and sorbitol, organic racids, such as acetic acid, fumaric acid, lactic acid, pyruvic acid, gluconic acid, formic acid, butyric acid and malic acid, lower alcohols such as ethanol and methanol, and hydrocarbons, etc. may be used.

As the nitrogen source, ammonia, inorganic and organic ammonium salts, such as ammonium chloride, ammonium sulfate, ammonium acetate, ammonium phosphate, ammonium carbonate and ammonium nitrate, urea, amines, other nitrogen-containing compounds such as peptone, meat extract, yeast extract, corn steep liquor, casein hydrolyzate, acid hydrolyzate of soybean meal, various microbial cells, digest of microbial cells, etc., may be used.

As the inorganic materials, potassium dihydrogen phosphate, dipotassium hydrogen phosphate, magnesium phosphate, magnesium sulfate, sodium chloride, ferrous sulfate, manganese sulfate, copper sulfate, calcium carbonate, etc. are used. Where a microorganism to be used in the present invention requires specific nutrients for growth, an appropriate amount of the nutrients is added to the medium. In some cases, these nutrients are added as components of the natural substances exemplified as the nitrogen source.

Further, the productivity of L-glutamic acid by a microorganism according to the present invention can be, in some cases, enhanced by adding other various additives, for example, various antibiotics such as streptomycln, penicillin G and rifampicin, antioxidant, such as  $\alpha$ -tocopherol, surfactants such as polyoxyethylene sorbitan-mono-parmitate, amino acids such as methionine, lysine, cysteine and aspartic acid, biotin, acetic acid, oleic acid, adenine, etc., to the medium.

Culturing is carried out under aerobic conditions, for example, by shaking culture, agitation submerged culture, etc. The temperature for culturing is generally 20-40°C, and the pH of the medium is in a range of 3 to 9, and is preferably maintained at around neutrality, but culturing can be carried out under conditions which are out of this range so long as the microorganism used can grow. The pH of the medium is adjusted with calcium carbonate, acid or alkali solution, ammonia, pH buffering agent, etc. Usually, after culturing for 1 to 4 days, L-glutamic acid is formed and accumulated in the resulting culture liquor.

After the completion of culturing, precipitates such as cells, are removed from the culture liquor and L-55 glutamic acid can be recovered from the culture liquor by use of the conventional methods, such as ionexchange resin treatment, concentration, adsorption and salting-out in combination.

Practice of specific embodiments of the invention is illustrated by the following representative examples.

#### Example 1

As seed strains, four strains of Corynebacterium glutamicum ATCC-13032 and COM-53 and Brevibacterium lactofermentum ATCC-13869 and BOM-419 are used.

As the seed medium, the medium (pH 7.2) having a composition of 4% glucose, 2% polypeptone, 0.5% yeast extract, 0.15% KH<sub>2</sub>PO<sub>4</sub>, 0.05% K<sub>2</sub>HPO<sub>4</sub>, 0.05% MgSO<sub>4</sub>.7H<sub>2</sub>O, 100 µg/l biotin and 0.3% urea, which has been sterilized at 120 °C for 10 minutes, is employed. The strains described above are cultured at 30 °C with shaking for 24 hours. Then, 1 ml of the culture liquor is inoculated into 20 ml of a fermentation medium described below which is charged in a 300 ml-Erlenmeyer flask. Culturing is carried out at 30 °C with shaking for 3 days. The results are shown in Table 1.

#### Composition of Fermentation Medium

15 10% glucose, 0.5% meat extract, 3% amminium sulfate, 0.15% KH<sub>2</sub>PO<sub>4</sub>, 0.05% K<sub>2</sub>HPO<sub>4</sub>, 0.05% MgSO<sub>4</sub>.7H<sub>2</sub>O, 500 μg/l of thiamine hydrochloride, 10 mg/l FeSO<sub>4</sub>.7H<sub>2</sub>O, 10 mg/l MnSO<sub>4</sub>.4-6H<sub>2</sub>O, 1 mg/l CuSO<sub>4</sub>.5H<sub>2</sub>O, 0.5% urea, 3% CaCO<sub>3</sub> (pH 7.2), sterilized at 120 °C for 10 minutes.

Table 1

20

25

Strain L-Glutamic Yield based on acid (g/l) sugar (%) ATCC-13032 49 49 **COM-53** 55 55 ATCC-13869 45 45 **BOM-419** 53 53

30

#### Example 2

The same procedures as described in Example 1 are repeated except that 10% (calculated as glucose) molasses is used in place of glucose as the fermentation medium in Example 1 and penicillin G solution is added to make a final-concentration of 5 U/ml at the initiation of the culturing. The results are shown in Table 2.

40

45

Table 2

Strain	L-Glutamic acid (g/l)	Yield based on sugar (%)
ATCC-13032	46	46
COM-53	52	52
ATCC-13869	41	41
BOM-419	47	47

50

55

#### Claims

1. A process for producing L-glutamic acid, which comprises culturing an L-glutamic acid producing microorganism belonging to the genus Corynebacterium or Brevibacterium in a nutrient medium until L-glutamic acid is accumulated in the resulting culture liquor, and recovering the L-glutamic acid therefrom, characterised in that the microorganism used has a resistance to one or more antibiotics of the type which

#### EP 0 350 970 A1

inhibit energy metabolism and selected from oligomycin, antimycin A, rutamycin, and valinomycin.

- 2. A process according to claim 1, wherein the microorganism used also has a resistance to one or more compounds being compounds which are precursors in the biosynthesis of ubiquinone.
- 3. A process according to claim 1 or 2, characterised in that the microorganism used is a strain of the species Corynebacterium glutamicum or Brevibacterium lactofermentum.
- 4. A process according to claim 3, characterised in that the microorganism is Corynebacterium glutamicum COM-53, FERM BP-428, or Brevibacterium lactofermentum BOM-419, FERM BP-429.
- 5. A process according to any one of the preceding claims, characterised in that the culture is conducted at 20 to 40 °C for 1 to 4 days.
- 6. A biologically pure culture of a microorganism having the identifying characteristics of:

  Corynebacterium glutamicum FERM BP-428, or

  Brevibacterium lactofermentum FERM BP-429.

## **EUROPEAN SEARCH REPORT**

EP 89 11 5775

Category	Citation of document with i of relevant pa	ndication, where appropriate, ssages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)
A	GB-A-2 056 451 (AJ * Whole document * 	INOMOTO CO. INC.)	1-6	C 12 P 13/14 C 12 N 1/20 // (C 12 N 1/20 C 12 R 1:13 C 12 R 1:15)
		•		TECHNICAL FIELDS SEARCHED (Int. Cl.4)
				C 12 P C 12 R
	The present search report has b	een drawn up for all claims		
	Piace of search HAGUE	Date of completion of the search 05-10-1989	CIID	Examiner IDO M.
X: par Y: par	CATEGORY OF CITED DOCUME ilcularly relevant if taken alone ilcularly relevant if combined with an ument of the same category inclogical background in-written disclosure irmediate document	NTS T: theory or prin E: earlier patent after the filin other D: document cite L: document cite	ciple underlying th document, but put g date ed in the application d for other reasons	ne invention blished on, or on s